

N₂O Laser Absorption Measurements During Toluene/N₂O Combustion

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1 Introduction

Using ammonia as a fuel is emerging as a possible solution to produce energy while mitigating carbon emissions and the associated global warming [1]. However, ammonia suffers from many drawbacks when used as a fuel; including a very slow flame speed and narrow flammability limits [2], and high ignition temperatures [3] compared to traditional hydrocarbon-based fuels. To lessen these issues, it is often considered to burn ammonia in a dual-fuel configuration. For instance, in internal combustion engines, several studies have considered ammonia/gasoline blends to power spark-ignition engines in passenger cars (see [4] and references therein).

In an internal combustion engine, due to the presence of residual gases from the previous combustion cycle, it is important to understand the interactions between the fresh charge and the combustion products from the previous cycles, which also include pollutants and unburned species. Notably, N₂O is an important combustion intermediate of ammonia combustion [5], for which emissions must be strictly limited due to its very high global warming potential of about 300 times that of carbon dioxide on a 100-year timescale. Furthermore, N₂O emissions are expected to remain the dominant ozone-depleting substance in the stratosphere throughout the 21st century [6].

Toluene is present in gasoline and is also generally considered as representative of the aromatic class of hydrocarbons present in gasoline. Studying the interactions between toluene and N₂O is therefore necessary for the efficient co-combustion of ammonia and gasoline in spark-ignition engines, especially because the literature is very limited for that system [7,8]. To address this gap, the aim of this study is to provide fundamental data for model validation. Specifically, the decomposition of N₂O was followed behind reflected shock waves using a laser absorption diagnostic during the oxidation of toluene by N₂O in highly dilutes mixtures. The results were compared to predictions from detailed kinetics models from the literature. To the best of our knowledge, there are only two groups producing models describing the oxidation of toluene with a detailed NO_x sub-mechanism: Curran's group at NUI Galway [9] and the CRECK group at POLIMI [10]. Note that Liang et al., 2024 also propose a model describing the interactions between gasoline and N₂O [11], but the hydrocarbon sub-mechanism is based on an earlier version of Curran group one and was thus not used herein.

2 Experimental setups

2.1. Shock Tube and Conditions Investigated

Experiments were conducted in the Aerospace Shock Tube (AST) at Texas A&M University. This facility is made of stainless-steel and set up for chemical kinetics measurements at low-to-intermediate pressure conditions using laser absorption experiments. The driver section has a 7.62-cm inner diameter and is 3.25 m long, while the driven section has a 16.2-cm inner diameter and is 7.88 m long. These two parts are separated by a single polycarbonate diaphragm and a cross-shaped cutting blade is used to facilitate the diaphragm’s rupture and initiate shock propagation.

To measure the incident-shock velocity, five piezoelectric pressure transducers (PCB P113A) were employed to detect non-intrusively the shock passage over the last 2 m of the shock tube. The temperature (T_5) and pressure (P_5) behind the reflected shock wave were calculated using a code based on the 1-D normal shock equations within uncertainties of $\pm 1\%$ and $\pm 0.8\%$, respectively. The shock tube has a vacuum system utilizing a rotary vane pump (Agilent DS 402) and a turbomolecular pump (Agilent Turbo V1001 Navigator) to achieve pressures of 10^{-8} atm or less prior to each test. Gas pressures are measured using capacitance manometers (MKS Baratron with 0 – 10 and 0 – 1000 Torr ranges). Optical windows ports are located at the same axial plane near the endwall to enable laser absorption measurements. Finally, three mixtures of toluene (C₇H₈) and nitrous oxide (N₂O) were studied in 0.2/0.79 He/Ar (He is typically added to expedite the vibrational relaxation, see [12] for more details) at three equivalence ratios ($\phi = 0.5, 1.0, \text{ and } 2.0$) for temperatures (T_5) and pressures (P_5) ranging from 1511 to 1868 K and from 1.20 to 1.32 atm, respectively. Table 1 provides the species mole fractions of the mixtures and summarizes the experimental conditions covered during the course of this study. Lastly, the liquid C₇H₈ comes from Sigma Aldrich with a purity of 99.8%, and all the gases were provided by Linde: N₂O with a purity $\geq 99\%$, He and Ar with 99.999% purity.

Table 1: Mixture composition and experimental conditions for C₇H₈/N₂O mixtures in 0.2/0.79 He/Ar.

ϕ	$X_{C_7H_8}$	X_{N_2O}	Temperature (K)	Pressure (atm)
0.5	0.00027	0.00973	1511 - 1820	1.21 – 1.30
1.0	0.000526	0.009474	1599 – 1868	1.20 – 1.32
2.0	0.001	0.009	1577 – 1804	1.20 – 1.29

2.2. N₂O Laser Diagnostic

A tunable quantum cascade laser (QCL), initially designed for CO absorption measurements, was tuned to monitor the N₂O decomposition behind reflected shock waves during the oxidation of toluene (C₇H₈) by N₂O. With a range of 2056 – 2064 cm⁻¹, the tunable QCL can access the P(128e) transition line of N₂O in the fundamental band ($1 \leftarrow 0$) at 2062.026 cm⁻¹. The calculations of the fractional absorbance, carried out using the HITEMP database [13] for N₂O in the tunable range, show a fairly good 15% absorbance with the following parameters: $X_{N_2O} = 9,000$ ppm, 1700 K, 1.3 atm, and a path length of 16.2 cm (shock-tube I.D.). Note that the laser absorption diagnostic is working in good isolation from the CO transition line, as well as common combustion intermediate products, such as H₂O and CO₂, to cite a few. The laser beam was divided into two distinct paths: the incident intensity I_0 and the transmitted intensity I_t passing through the reacting gases in the shock tube. Both are collected separately by two InSb detectors after passing a direct-absorption setup consisting of lenses and bypass filters (Thorlabs). The wavelength was centered and verified before each test with a flip mirror sending the light into a wavemeter (Bristol 671). Finally, the time-resolved N₂O mole fractions are calculated with these two intensities (I_0 and I_t) using the Beer-Lambert relation, defined as $I_t/I_0 =$

$\exp(-k_v PLX_{N_2O})$, where k_v is the absorption coefficient, P is the pressure, L is the path length (shock-tube I.D.), and X_{N_2O} is the N₂O mole fraction. The absorption coefficient was calibrated for a large range of temperatures and pressures, namely 710 – 1392 K near 0.205 – 0.406 atm using T_2 , P_2 (Low temperature, LT) and 1225 – 1904 K near 1.13 – 1.59 atm using T_5 , P_5 (High temperature, HT) as can be seen in Fig. 1. For the current experiments, the calibration using T_5 and P_5 is needed and is described using Eqn. 1 and 2 for the highest temperatures (1700 – 1900 K).

$$k_{v,LT} = 5.273 \times 10^{15} \times T^{-4.8961} \quad (1)$$

$$k_{v,HT} = 5.964 \times 10^6 \times T^{-2.0201} \quad (2)$$

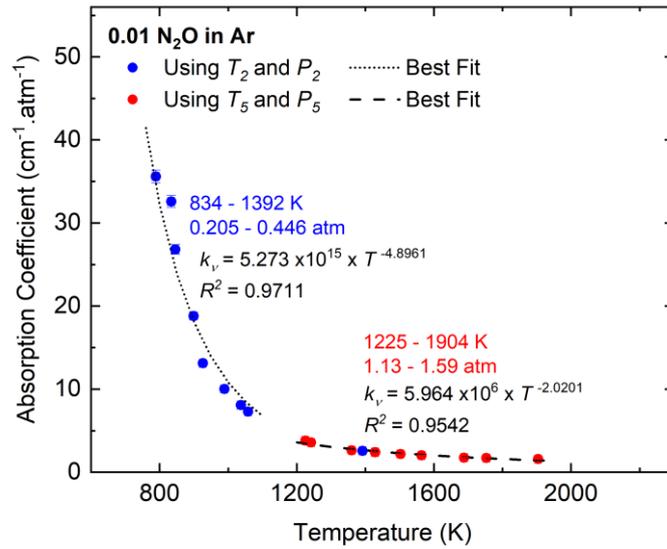


Figure 1: Characterization of the temperature dependence of the absorption coefficient for 0.01 N₂O in Ar using the P(128e) transition line of N₂O in the fundamental band ($1 \leftarrow 0$) at 2062.026 cm⁻¹. Data were taken at T_2 , P_2 (710 - 1392 K, 0.205 - 0.446 atm), and T_5 , P_5 (1225 - 1904 K, 1.13 - 1.59 atm).

A mixture of N₂O in 0.99 Ar was studied behind reflected shock waves to obtain the calibration results and characterize the absorption capability of the P(128e) transition line of N₂O in a bath of Ar. An uncertainty analysis, where the root sum square method was done, consisted in perturbing several factors that are part of the k_v calculations and noting the change that echoes in the final k_v . Three parameters are considered in this study: P ($\pm 1\%$), L (± 0.1 cm), and X_{N_2O} ($\pm 3\%$, based on [22]) that induce a difference of 1%, 0.6%, and 3%, respectively, leading to a 4.6% total uncertainty on k_v , and on the N₂O mole fraction. During the experiments, the exothermicity from the reaction of C₇H₈ with N₂O induces an increase in the temperature T_5 during the process. These changes in temperature were accounted for using Eqns. 1 and 2, creating an adapted time-varying absorption coefficient with the temperature variation predicted by the current model presented herein. The high dilution was chosen to keep the temperature change below 150 K ($\Delta T = 80 - 120$ K), minimizing any uncertainties from the temperature predictions of the model.

3 Experimental Results and Model Comparison

The N₂O profiles obtained during this study are visible in Fig. 2 for (a) $\phi = 0.5$, (b) $\phi = 1.0$, and (c) $\phi = 2.0$. For the fuel-lean case, no apparent consumption of N₂O is observed for the coldest temperature investigated, 1511 K, within the time frame of the experiment. Above this temperature, the N₂O mole fraction starts decreasing right from the beginning of the experiment. Increasing the temperature leads to a faster consumption of N₂O, although it is worth mentioning that the N₂O mole fraction never reaches

zero in our conditions. For the stoichiometric and fuel-rich mixtures, similar observations can be made except that the mole fraction reaches zero for these mixtures. Moreover, for the coldest temperatures investigated with the stoichiometric mixtures, a rapid change in the rate of N₂O consumption can be observed at around 1500 μ s and 2000 μ s for the 1619 K and 1599 K cases, respectively, indicating a possible change in the consumption pathway. Note that comparing the three equivalence ratios at similar temperatures (1690 K, 1694 K, and 1707 K, and 1596 K, 1599 K, and 1581 K for $\phi = 0.5, 1.0,$ and $2.0,$ respectively) does not show major differences between the profiles, except the aforementioned change in the consumption rate at 1599 K, $\phi = 1.0$. This indicates that the N₂O consumption is relatively independent of the equivalence ratio in our conditions. These results and observations will be discussed using the NUIG model in the next section.

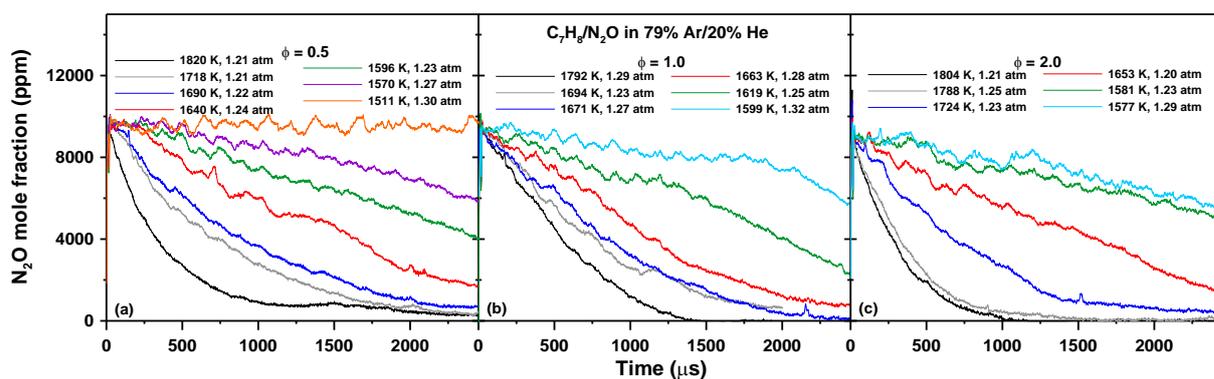


Figure 2: Evolution with time of the N₂O mole fraction during the oxidation of toluene by N₂O for mixtures diluted in 99% Ar and He. (a) $\phi = 0.5$, (b) $\phi = 1.0$, and (c) $\phi = 2.0$.

4 Model Comparison and Discussion

Selected N₂O profiles on the low- and high-temperature extremes of the ranges investigated were compared to the model predictions in Fig. 3. Overall, the fuel-lean mixture is well predicted by the models, notably by the NUIG model at low temperature. On the other hand, both models predict a full consumption of N₂O at high temperature, which is not observed experimentally. For the stoichiometric case, both models tend to be over-reactive over the entire range of temperatures investigated, with the NUIG model being the closest to the data. Note that the change of slope in the N₂O consumption observed experimentally is also seen for the models, although the change is not as abrupt as for the experiment. Lastly, for the fuel-rich case, the models are still relatively close to the data but they tend to be under-reactive, especially for the NUIG model.

A numerical analysis based on rate of production and reaction pathway analyses was conducted using the NUIG model to understand better the results. Under our conditions, the reactivity is actually initiated by the thermal decomposition of toluene, forming the radical H and the benzyl radical (C₆H₅CH₂). This H radical will then attack the N₂O to form OH via $\text{N}_2\text{O} + \text{H} \rightleftharpoons \text{N}_2 + \text{OH}$, with also a strong contribution from the thermal N₂O decomposition via $\text{N}_2\text{O} (+\text{M}) \rightleftharpoons \text{N}_2 + \text{O} (+\text{M})$ with regards to N₂O consumption. Note that all these radicals H, OH, and O also then attack toluene and its combustion intermediates. The fact that N₂O consumption essentially only depends on the initial decomposition of toluene and on the thermal dissociation of N₂O explains why the N₂O profiles are relatively insensitive to the equivalence ratio under our conditions.

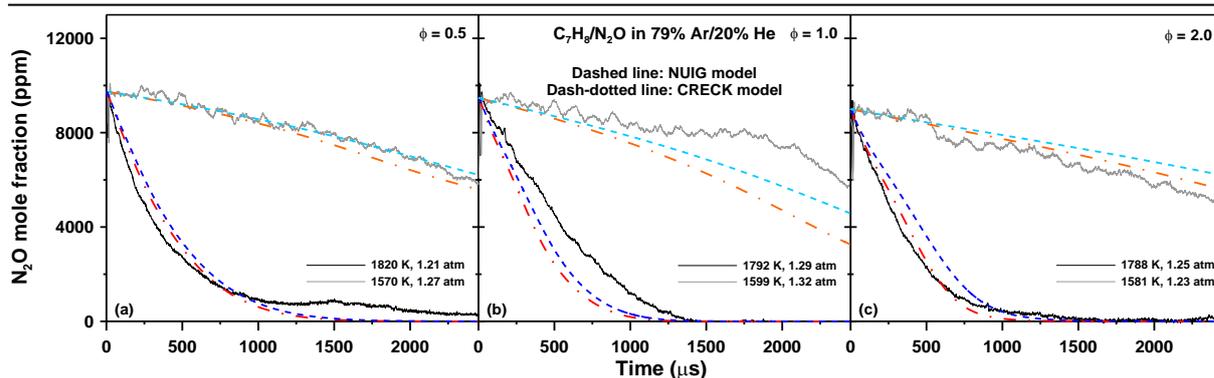


Figure 3: Evolution with time of the N₂O mole fraction during the oxidation of toluene by N₂O for mixtures diluted in 99% Ar and He and comparison with models from the literature. (a) $\phi = 0.5$, (b) $\phi = 1.0$, and (c) $\phi = 2.0$.

5 Conclusions

The time history of N₂O was followed by laser absorption spectroscopy during the combustion of toluene/N₂O mixtures for the first time. The data are useful for validating kinetics models for the development of spark ignition engines using a dual fuel setup with gasoline and ammonia. Results showed that the N₂O consumption varies greatly with the temperature but is weakly impacted by the equivalence ratio under the conditions investigated.

Models from the literature were generally capable of reproducing the data but room for improvement remains, especially for the stoichiometric and fuel-rich cases. A numerical analysis showed that the reactivity is initiated by the fuel thermal decomposition, leading to the formation of H and benzyl radicals. These H radicals will then react with toluene or N₂O to initiate the N₂O consumption by forming OH and nitrogen. This pathway is the preferred N₂O consumption pathway under our conditions, but a large contribution is also coming from the thermal decomposition of N₂O.

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